Direct numerical simulation of turbulent flows over acoustic liners



EuroHPC

Project: "ENTRAIN"

EuroHPC used: Meluxina

Speaker: Davide Modesti (TU Delft)

Introduction

Pre-exascale EU supercomputers



Rank	System	RPeak (ExaFlop/s)	Power (MW)
1.	Frontier (US)	1.6	23
2.	Aurora (US)	1.0	25
5.	LUMI (Finland)	0.4	7
6.	Leonardo (Italy)	0.3	7

The flow solver: STREAmS-2



Documentation: https://streams-cfd.github.io/STREAmS-2/

Github: https://github.com/STREAmS-CFD/STREAmS-2

Main features:

- Open source GPL-3.0 license
- Direct numerical simulation of wall bounded fows
- Three different backends: CPU, NVIDIA GPU, AMD GPU
- Object oriented framework, modern Fortran

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- 🔽 @streams_cfd
- @streamscfd6365
- 🗮 streamsdns



Developers team



Davide Modesti, TU Delft

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Srikanth Sathyanarayana, MPC

Sergio Pirozzoli, Sapienza

Research topics:

- Turbulent high-speed flows
- Wall turbulence
- Aeroacoustics
- Numerical methods
- High performance computing

STREAmS-2: numerics



Discretization:

- Hybrid energy conserving/shock capturing finite difference¹
- High order WENO reconstruction close to discontinuities
- Arbitrary order of accuracy for spatial derivatives
- Explicit time step integration, 3rd order low storage R-K

¹S. Pirozzoli J. Comput. Phys. 229.19 (2010): 7180-7190.



Haris Shahzad Stefan Hickel TU Delft











$$\begin{split} u_{\tau} &= \sqrt{\tau_w/\rho_w} \\ \delta_v &= \nu_w/u_{\tau} \\ \textit{Re}_{\tau} &= \delta/\delta_v \\ C_f &= 2\tau_w/(\rho_{\infty}u_{\infty}^2) \end{split}$$



$$u_{\tau} = \sqrt{\tau_w/\rho_w}$$

$$\delta_v = \nu_w/u_{\tau}$$

$$Re_{\tau} = \delta/\delta_v$$

 $\begin{array}{l} k/\delta << 1 \\ k^+ = k/\delta_v >> 1 \\ k^+ > 5 \text{ rough wall} \end{array}$



$$u_{\tau} = \sqrt{\tau_w/\rho_w}$$

$$\delta_v = \nu_w/u_{\tau}$$

$$Re_{\tau} = \delta/\delta_v$$

 $\begin{array}{ll} k/\delta <<1 & & \\ k^+=k/\delta_v>>1 & & \\ k^+>5 \mbox{ rough wall } & & \\ \end{array} \qquad \begin{array}{ll} d/\delta=? & \\ d^+=d/\delta_v=? \end{array}$



Noise reduction of about 8–10dB $d/\delta \approx 0.1$ $d^+ = d/\delta_v \approx 120$ –500 $\sigma = 0.08$ –0.3













Effect of roughness: review



$$\sum_{k^+ = k/\delta_v}^{C} \sum_{k^+ = k/\delta_v}^{C} \delta_v$$







$$\sum_{k^+ = k/\delta_v}^{C} \sum_{k^+ = k/\delta_v}^{C} \delta_v$$



$$\frac{\delta_{v}}{k^{+} = k/\delta_{v}}$$

	d^+	σ	ΔD
GFIT ^{2,3,4}	180 - 660	0.08 - 0.3	10 - 350%
Wilkinson (1983) ⁵	9 - 150	0.047 - 0.14	2-60%
Gustavsson et al. (2019) ⁶	350 - 550	0.0853	30-50%
Zhang and Bodony (2016) ⁷	114	0.0099	4-100%
Scalo <i>et al.</i> (2015) ⁸	Imped	ance B.C	$\leq 325\%$
Sebastian <i>et al.</i> $(2019)^9$	Imped	ance B.C	$\leq 575\%$

²B.M. Howerton and M.G. Jones (2015), AIAA Paper 2015-2230
³B.M. Howerton and M.G. Jones (2016), AIAA Paper 2016-2979
⁴B.M. Howerton and M.G. Jones (2017), AIAA Paper 2017-4190
⁵Wilkinson (1983), AIAA Paper 1983-0294
⁶Gustavsson *et al.* (2019), AIAA Paper 2019-2683
⁷Q. Zhang and D.J. Bodony (2016), J. Fluid Mech. 792, pp 936–980
⁸C. Scalo, J. Bodart, S.K. Lele (2015). Phys. Fluids 27.3, p. 035107
⁹R. Sebastian, D. Marx, and V. Fortuné (2019), J. Sound Vib. 306–330

DNS of turbulent channel flow Domain size $3\delta \times 2(\delta + h) \times 1.5\delta$ Bulk Mach number $M_b = 0.3$





 $Re_b \qquad Re_\tau \qquad d^+ \qquad \sigma \qquad t/d \quad 1/\alpha^+ \qquad \Delta x^+ \quad \Delta y^+_{\min} \quad \Delta z^+$

L_1 9139 503.5 40.3 0.0357 1 0.0528 1.1 0.80 1.1



	Re_b	Re_{τ}	d^+	σ	t/d	$1/\alpha^+$	Δx^+	Δy_{\min}^+	Δz^+
L_1	9139	503.5	40.3	0.0357	1	0.0528	1.1	0.80	1.1
L_2	8794	496.4	39.7	0.142	1	0.859	1.0	0.80	1.0
-									
L_A	19505	1038	83.0	0.142	1	1.80	2.1	0.81	2.1
4									



	Re_b	Re_{τ}	d^+	σ	t/d	$1/\alpha^+$	Δx^+	$\Delta y^+_{\rm min}$	Δz^+
L_1	9139	503.5	40.3	0.0357	1	0.0528	1.1	0.80	1.1
L_2	8794	496.4	39.7	0.142	1	0.859	1.0	0.80	1.0
2									
L_3	8264	505.3	40.4	0.322	1	5.14	1.0	0.81	1.0
	19505	1038	83.0	0.142	1	1.80	2.1	0.81	2.1
L_4	19505	1056	85.0	0.142	1	1.00	2.1	0.01	2.1
т	17010	1026	90 1	0.222	1	10.4	0.1	0.02	0.1
L_5	1/810	1026	82.1	0.322	I	10.4	2.1	0.82	2.1
_									
L_6	35470	2044	164.0	0.322	1	20.8	4.1	0.82	4.1

 	_	 _	-	-	_	

	Re_b	Re_{τ}	d^+	σ	t/d	$1/\alpha^+$	Δx^+	Δy_{\min}^+	Δz^+
L_1	9139	503.5	40.3	0.0357	1	0.0528	1.1	0.80	1.1
L_{t1}	9139	508.8	40.7	0.0357	0.5	0.0533	1.5	0.81	1.1
L_2	8794	496.4	39.7	0.142	1	0.859	1.0	0.80	1.0
L_{t2}	8794	520.8	41.6	0.142	0.5	0.901	1.6	0.83	1.1
L_3	8264	505.3	40.4	0.322	1	5.14	1.0	0.81	1.0
L_4	19505	1038	83.0	0.142	1	1.80	2.1	0.81	2.1
L_{t4}	19505	1031	82.5	0.142	0.5	1.78	3.1	0.82	1.1
L_5	17810	1026	82.1	0.322	1	10.4	2.1	0.82	2.1
L_{t5}	17810	1057	84.6	0.322	0.5	10.7	3.2	0.85	1.1
L_6	35470	2044	164.0	0.322	1	20.8	4.1	0.82	4.1

	Re_b	Re_{τ}	d^+	σ	t/d	$1/\alpha^+$	Δx^+	Δy_{\min}^+	Δz^+
S_1	9268	506.1	0	0	0	0	5.1	0.80	5.1
S_2	21180	1048	0	0	0	0	5.2	0.80	5.2
S_3	45240	2060	0	0	0	0	5.2	0.80	5.2
L_1	9139	503.5	40.3	0.0357	1	0.0528	1.1	0.80	1.1
L_{t1}	9139	508.8	40.7	0.0357	0.5	0.0533	1.5	0.81	1.1
L_2	8794	496.4	39.7	0.142	1	0.859	1.0	0.80	1.0
L_{t2}	8794	520.8	41.6	0.142	0.5	0.901	1.6	0.83	1.1
L_3	8264	505.3	40.4	0.322	1	5.14	1.0	0.81	1.0
L_4	19505	1038	83.0	0.142	1	1.80	2.1	0.81	2.1
L_{t4}	19505	1031	82.5	0.142	0.5	1.78	3.1	0.82	1.1
L_5	17810	1026	82.1	0.322	1	10.4	2.1	0.82	2.1
L_{t5}	17810	1057	84.6	0.322	0.5	10.7	3.2	0.85	1.1
L_6	35470	2044	164.0	0.322	1	20.8	4.1	0.82	4.1

Instantaneous flow field channel flow



Instantaneous flow field channel flow



Instantaneous flow field channel flow

Instantaneous velocity in a wall-parallel plane at $y^+ = 12$, $Re_\tau = 2044$



Turbulent boundary layer over acoustic liners¹⁰



Added drag

 ΔU^+ depends on wall-normal permeability of the plate¹¹ ¹².



¹¹H. Shahzad, S. Hickel, D. Modesti Flow Turbul. Combust. 109.4 (2022): 1241-1254.
 ¹²H. Shahzad S. Hickel D. Modesti J. Fluid Mech. 965 (2023): A10.
Acoustic liners: optimized geometries



Acoustic liners: optimized geometries Acoustic Performance

No grazing flow, array of 40 cavities¹³



¹³H. Shahzad, S. Hickel, D. Modesti AIAA J. (Under review)

Acoustic liners: optimized geometries

SPL Loss



Acoustic liners: optimized geometries

SPL Loss





Ongoing work

Broadband acoustic liners



Ongoing work

Turbulent boundary layer with incoming sound wave, currently running on Meluxina



Final Remarks

- STREAmS-2 targets CPU and multiple GPU backends
- DNS at engineering Reynolds numbers are becoming accessible
- EuroHPC facilities are key



Final Remarks

Interview for the general public

Science | Mechanics + ... | 2022

Quiet Query: Scientists model how noise-reducing aircraft liners are a drag on efficiency

Aircraft noise is reduced by acoustic liners covering the inner surfaces of its engines. However, these components also add to aerodynamic drag — but by how much, and how this can be mitigated, was unclear. Thanks to simulations performed on the CSCS supercomputer "Piz Daint", scientists have now deciphered the acoustic liners' impact and how to improve them.

November 21, 2022 - by Santina Russo



QR code



Scale-resolving flow simulations for gaining physical insight in the flow and improving turbulence models for turbomachinery applications



Projects: RoundedStepData4ML + BE share on LUMI + Early access on LUMI + TurbData4ML (PRACE) EuroHPC used: VEGA@IZUM, LUMI@CSC Speaker: Michel RASQUIN (Cenaero)

High-fidelity CFD @ Cenaero

Author list: M. Rasquin, T. S. Cação Ferreira, T. Toulorge, K. Hillewaert

Cenaero





- High-resolution DNS and wall-resolved LES on realistic geometries
 - Accurate representation of flow phenomena in boundary layers near solid surfaces
 - Separation
 - Shocks
 - Transition and turbulence
 - Main enablers

PROD-F-015-02

- Superior accuracy of high-order methods like DGM
- Access to and efficient exploitation of supercomputers



- **Research themes for the application of DNS and LES**
 - **Development of high-resolution numerical methods & tools**
 - Applications: high fidelity CFD of complex flows
 - High-pressure turbine vane LS89
 - **Data-driven turbulence modeling**
 - HiFi-Turb-DLR rounded step





Development of high-resolution numerical tools *Highly accurate numerical wind tunnel for turbulence in turbomachinery*

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High-order Discontinuous Galerkin Method Why DG?

- Unstructured meshes and complex geometries
- High accuracy
 - Guaranteed order of convergence p+1
 - No degradation near size jumps/walls
 - Low dissipation/dispersion error
- High efficiency

PROD-F-015-02

- Data locality
- Compact matrix-matrix operations
- High scalability (MPI/OpenMP/GPU)





Aircraft gas turbine engine High pressure turbine vane LS89



- 2021 PhD thesis Tânia Sofia Cação Ferreira + follow up
- **Boundary layer transition and** convective heat transfer of the high-pressure turbine vane LS89 **Complementary experimental** and numerical work

High-pressure turbine







High-pressure aircraft gas turbine Highest temperature during engine cycle



DNS of an isothermal and reacting combustion swirler (Moureau et al. 2010)



Combustor exit/HPT inlet flow:

- Temperature = 500-2000K
- Turbulence intensity = 10-30%

1st turbine stator

faces the hot turbulent combustion flow

- Accurate heat transfer predictions are <u>crucial</u> for efficiency and safety!
- Requires accurate prediction of the boundary layer

Domain and boundary conditions MUR235/TUR87 configuration



Heat transfer Results



Observations:

- Experiments: highly sensitive boundary layer to the facility environment
- Simulations: strong dependence on the mesh resolution (and on the artificial viscosity)
- 2nd experimental campaign with updated facility (TUR87) and refined numerical simulations tend to converge towards the same heat flux prediction

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Flow visualisation Density gradient



Acoustic waves reflection on the suction side

Wake vortex shedding

Acoustic waves formation at the trailing edge

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Normal shock



Refined inlet turbulent structures

Heat transfer Mesh M2





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Data-driven turbulence modeling Generic methodology



HiFi-Turb-DLR rounded step Test case definition

- Test case proposed within H2020 HiFi-Turb project
 - Documented in the ERCOFTAC Knowledge Base wiki
 - <u>https://www.kbwiki.ercoftac.org/w/index.php/DNS_1-5</u>
- Features an adverse pressure gradient on a turbulent boundary layer
 - 3 step heights
 - Incipient, moderate (Re_h=98113) and full separation





HiFi-Turb-DLR rounded step Mesh characteristics

	Incipient	Moderate	Full
Hexes	10.3 M	10.8 M	11.6 M
Dof	1.30 B	1.35 B	1.45 B
Height (m)	2.90e-2	3.62e-2	4.38e-2
Span (m)		8.69e-2	
Span/height	3	2.4	2
Nz	188		
Δz	4.10e-4 m		
Upstream bump			
Δx ⁺	<20		
Δy ₁ +	<1		
Δz+	<14.8		
Bump			
Δx	*0.5 w.r.t. upstream bump		





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Flow visualisation *Wall shear stress* + *Vorticity*











Summary

- High-resolution simulations as part of a "multi-fidelity" paradigm
 - Physical understanding to support and complement experimental testing
 - Performance prediction in off-design conditions
 - Data generation for lower-fidelity model calibration (RANS, wall models)
- Advanced numerical framework
 - High-order numerical scheme
 - Scalable
 - Post-processing and statistical analysis
- Applications
 - Academic aerodynamic flows
 - Turbomachinery flows







Access to large computational resources is essential



- We acknowledge **EuroHPC JU** for awarding us access to
 - LUMI hosted by CSC in Kajaani, Finland
 - VEGA hosted by IZUM in Maribo, Slovenia
- We acknowledge **PRACE** for awarding us access to
 - Galileo hosted by CINECA in Bologna, Italy
 - Hawk hosted by HLRS in Stuttgart, Germany
- The present research benefited from computational resources made available on the Tier-1 supercomputer of the Fédération Wallonie-Bruxelles, infrastructure funded by the Walloon Region under grant agreement numbers 1117545 and 1910247



Thank you for your attention





A Portable Drug Discovery Platform for Urgent Computing



Project: EHPC-BEN-2022B12-001

EuroHPC used: LUMI-G

Speaker: Davide GADIOLI (Politecnico di Milano)



Drug discovery

- Target at least one protein that represents the disease
- The goal is to find a small molecule that has a strong interaction
 - Expected to yield a therapeutic effect in clinical trials

Virtual screening

Problem input

- Target protein
- Huge databse of virtual molecules

Expected output

• Molecules to test in-vitro





Why High Performance Computing?

- The interaction strength estimation is complex
- The evaluation of each molecule-protein pair is independent
 Embarrassing parallel problem
- Simulation of known chemical reactions grants access to huge chemical space
 o increasing the probability of finding good candidates

LiGen Virtual Screening Application

- Component of the EXSCALATE drug discovery platform
- Designed from scratch to hinge on modern supercomputer nodes
- Used to perform extreme-scale virtual screening campaign





Dompé





HPCaaS: The Urgent Computing Scenario

- LiGen deployed on multiple EU HPC centers
- Integration in the LEXIS platform
- Virtual screening on multiple locations





Manage Hardware Heterogeneity

- Efficient CUDA implementation
 - Support from NVIDIA engineers
- We introduced a SYCL porting
 - Computation kernels
 - Out-of-order input computation





LiGen Computation parallelism





LiGen Batched Approach

1. Write kernels with non-type template parameters for atom number

• Different hardware requirements

```
template<size_t num_atoms>
__global__ void kernel( ... ) {
   ...
}
```



LiGen Batched Approach

- 1. Write kernels with non-type template parameters for input features
- 2. Define input features clusters that impact the kernel's complexity
 - The ligands computation should last for a similar period



LiGen Batched Approach

- 1. Write kernels with non-type template parameters for input features
- 2. Define input features clusters that impact the kernel's complexity
- 3. Use Hardware characteristics to size each ligand batch at runtime
 - Automatic tuning using CUDA or SYCL query API


Performance on the single logical GPU card





Scaling on the number of GPUs (LUMI-G)

Num nodes	Num GPUs/node	Throguhput [molecule/s]	Speed-up
16	1	7'808.96	1
16	8	60'566.672	7.756

Strong Scaling on the number of nodes (LUMI-G)



NOTE: due to a technical problem with the FS, we used only 1 GPU per node



Acknowledgement

EuroHPC JU for awarding this project access to LUMI and Karolina

- We could optimize LiGen software-knobs
- We benchmarked on the LUMI machine
 - Ready to run a virtual screening campaign
- In the LIGATE context, we can provide access to LiGen through the LEXIS platform

References



- "EXSCALATE: an extreme-scale virtual screening platform for drug discovery targeting polypharmacology to fight SARS-CoV-2." IEEE Transactions on Emerging Topics in Computing
- "Understanding the I/O impact on the performance of high-throughput molecular docking." 2021 IEEE/ACM Sixth International Parallel Data Systems Workshop (PDSW).
- "Exploiting OpenMP and OpenACC to accelerate a geometric approach to molecular docking in heterogeneous HPC nodes." The Journal of Supercomputing
- "Improving computation efficiency using input and architecture features for a virtual screening application", arxiv, minor revision
- "GPU-optimized Approaches to Molecular Docking-based Virtual Screening in Drug Discovery: A Comparative Analysis", arxiv, minor revision

Large Eddy Simulations (LES) of a Three-Element High-Lift Wing: Exploring the Active Flow Control (AFC) Capabilities.



EuroHPC

Project: "Active Flow Control of a 3-Element High-Lift Wing: The Role of Coherent Structures"

EuroHPC used: Vega CPU (IZUM)

Motivation

GOAL



[1] European Environment Agency, Greenhouse gas emissions from transport in Europe, accessed 6 June 2023, <u>https://www.eea.europa.eu/ims/greenhouse-gas-emissions-from-transport</u>

[2] B. Eiximeno, A. Miró, J.C. Cajas, O. Lehmkuhl, I. Rodriguez (2022). DOI: https://doi.org/10.3390/fluids7090292

[3] O. Lehmkuhl, A. Lozano-Durán, I. Rodriguez (2020). DOI: <u>10.1088/1742-6596/1522/1/012017</u>



Motivation

GOAL



LES simulations of the baseline configuration



[1] European Environment Agency, Greenhouse gas emissions from transport in Europe, accessed 6 June 2023, <u>https://www.eea.europa.eu/ims/greenhouse-gas-emissions-from-transport</u>

[2] B. Eiximeno, A. Miró, J.C. Cajas, O. Lehmkuhl, I. Rodriguez (2022). DOI: https://doi.org/10.3390/fluids7090292

[3] O. Lehmkuhl, A. Lozano-Durán, I. Rodriguez (2020). DOI: <u>10.1088/1742-6596/1522/1/012017</u>

Understand the underlying physics of the problem



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Baseline LES – Case Configuration







Baseline LES – Validation



Skin Friction Coefficient(C_f)



[6] M. Murayama, K. Nakakita, K. Yamamoto, H. Ura, Y. Ito, M. Choudhari (2014). DOI: https://doi.org/10.2514/6.2018-3460

[7] K. Pascioni, L.N. Cattafesta, M. Choudhari (2014). DOI:<u>https://doi.org/10.2514/6.2014-3062</u>

[8] S. Klausmeyer, J. Lin (1994).
 DOI: <u>https://doi.org/10.2514/6.1994-1870</u>

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Baseline LES – Validation



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Skin Friction Coefficient(C_f)



 [6] M. Murayama, K. Nakakita, K. Yamamoto, H. Ura,
 Y. Ito, M. Choudhari (2014). DOI: <u>https://doi.org/10.2514/6.2018-3460</u>

[7] K. Pascioni, L.N. Cattafesta, M. Choudhari (2014). DOI:<u>https://doi.org/10.2514/6.2014-3062</u>

[8] S. Klausmeyer, J. Lin (1994). DOI:<u>https://doi.org/10.2514/6.1994-1870</u>

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Baseline LES – Flow Overview

Q-criterion isocontours at $lpha=5^{\circ}$

Streamlines Coloured by Velocity Magnitude





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 $\alpha = 5^{\circ}$

 $\alpha = 9^{\circ}$

 $\alpha = 23^{\circ}$



Baseline LES – Slat Cove Dynamics





Baseline LES – Slat Cove Dynamics

 10^{-1} α [°] St [-] 10-2 E_{pp}U_∞/p_∞²c 10 10 70 5 9 64 10^{-6} Kelvin-Helmholtz 23 35 10^{-7} Instabilities 10⁻⁸↓ 10⁰ 101 10² 10³ St

Pressure Spectra at P1

RMS of Cp'









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0.18

0.18

0.2

0.2

0.22

0.22





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Skin Friction Coefficient







Skin Friction Coefficient

Velocity Magnitude Spectra at P2







Skin Friction Coefficient



Velocity Magnitude Spectra at P2



Instantaneous TKE



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x/c



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Baseline LES – Trubulent Boundary Layer

$$\alpha = 5^{\circ}$$
 $\alpha = 9^{\circ}$ $\alpha = 23^{\circ}$







Baseline LES – Trubulent Boundary Layer



Momentum Thickness Reynolds







Baseline LES – Trubulent Boundary Layer



Clauser Pressure-Gradient Parameter



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Momentum Thickness Reynolds



Shape Factor



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AFC LES – Case Configuration



$$\begin{bmatrix} u \\ v \\ w \end{bmatrix}_{xyz, act} = U_{\infty} \sqrt{\frac{c}{h}} \boldsymbol{C}_{\mu} \sin\left(2\pi \frac{\boldsymbol{F}^{+} U_{\infty}}{L_{ref}} t\right) \begin{bmatrix} \cos(\boldsymbol{\varphi} - \theta_{0}) \\ \sin(\boldsymbol{\varphi} - \theta_{0}) \\ 0 \end{bmatrix} = \boldsymbol{f}(\boldsymbol{C}_{\mu}, \boldsymbol{F}^{+}, \boldsymbol{\varphi})$$

$Re_c = 750,000$ $\alpha = 23^{\circ}$	CASE ID	Main Actuation		Flap Actuation			
		Cμ	F ⁺	φ	C _μ	F^+	φ
	1	0.015	0.34	20 °	- Not actuated -		
	2	- Not actuated -		0.025	0.34	20°	
	3	0.015	1.52	90°	- Not actuated -		
	4	- Not actuated -		0.025	1.52	90°	
	5	0.015	1.52	45°	0.025	1.52	90°





AFC LES - Results

Case ID 1

Case ID 5



Work in Progress!





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Conclusions

- Computational data shows **good agreement** with the experimental observations.
- Evolution of flow dynamics **at increasing** α:
 - Slat SL: (i) Smaller recirculation area. (ii) Lower K-H frequencies. (iii) Weaker impingement strength. (iv) More pronounced wake (TBL on suction side).
 - Main turb. transition: (i) Nearly at constant locations. (ii) Higher T-S frequencies.
 - Main TBL: (i) Stronger APG. (ii) More pronounced main wake. (iii) Recirculation region (Stall conditions).
- Viscous drag remains nearly constant with α (from C_{d visc.} = 0.0114 to 0.0118); while pressure drag increases noticeably (from C_{d press.} = 0.0580 to 0.1865).
- Pressure is the main contributor to drag (Half or even one order of magnitude higher):
 - Flap has the highest $C_{d \text{ press.}}$ at lower α (curvature \rightarrow APG), but it remains approximately constant with α (constrained flow \rightarrow main-flap gap jet).
 - In the **slat**, $C_{d \text{ press}}$ diminishes with α (Higher suction peak + element inclination \rightarrow Positive force).
 - The C_{d press.} in the **main** goes from the lowest value (behaves nearly as a flat plate) to the highest one (Strong APG along suction side).
- Two actuations strategies tested with the idea of:
 - **Main actuator:** Reduce the APG in the main TBL \rightarrow reduce its wake.
 - Flap actuator: Increase the vertical mixing of the main-flap gap jet flow.



Future Work

- Analyse the **AFC results** and assess the differences with the baseline case: Why /Why not improved?
- Build **ROMs models** (POD, DMD, Autoencoders...): Fruther understand the Flow features contributed by the actuations.
- **Exploit** the capabilities of machine learning (**Deep Reinforcement Learning**) to optimize the actuation parameters.





Thank you for your attention











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Barcelona Supercomputing Oppter Centro Nacional de Supercomputación



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EuroHPC JU – User Day 2023 11th December 2023, Brussels (*Belgium*)

Heat-transfer in drop-laden turbulence





Project: "BubbLe-modUlated Mixing in turbulENce (BLUMEN)"

EuroHPC used: Discoverer

Speaker: Alessio ROCCON (Univ. Udine)



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The problem involves a wide range of spatial and temporal scales:

- Largest scale of problem
- Kolmogorov scale
- Molecular scale of the interface



Problem considered Multiphase turbulence









How does a passive scalar (e.g. temperature) behave in multiphase turbulence? Internal/external turbulent transport and turbulence-interface interactions can modify the mixing:

Breakage:



Heat transfer **Coalescence & breakage**

Interfacial area, temperature, relaxation times









Flow:

Assumptions:

- Same density/viscosity
- Small temperature difference
- Same thermal diffusivity

$$\nabla \cdot \mathbf{u} = 0$$

$$\rho(\phi) \left[\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right] = -\nabla p + \frac{1}{Re_{\tau}} \nabla \cdot \left[\eta(\phi) (\nabla \mathbf{u} + \nabla \mathbf{u}^{T}) \right] + \frac{3}{\sqrt{8}} \frac{Ch}{We} \nabla \cdot \tau_{c}$$
Interface:
$$\frac{\partial \phi}{\partial t} + \mathbf{u} \cdot \nabla \phi = \frac{1}{Pe_{\phi}} \nabla^{2} \mu_{\phi}$$
Surface tension forces



$$\frac{\partial \theta}{\partial t} + \mathbf{u} \cdot \nabla \theta = \frac{1}{Re_{\tau}Pr} \nabla^2 \theta$$

Cahn and Hilliard ,Free energy of a non-uniform system I, Interfacial free energy, JCP (1958) Roccon et al., "Phase-field modeling of complex interface dynamics in drop-laden turbulence, PRF (2023). Mangani et al., "Heattransfer in drop-laden turbulence", JFM (2023)

Multiphase turbulence Governing equations

Prandtl number

$$Pr = \frac{\nu}{a} = \frac{\text{Momentum diffusivity}}{\text{Thermal diffusivity}}$$

Transport equation for a passive scalar, no feedback on NS









The **Cahn-Hilliard equation** is the principal governing equation in the phase-field method and includes all important physical phenomena: **phase-change and surface tension**. CH equation is a fourth-order non linear partial differential equation.

$$\frac{\partial \phi}{\partial t} + \mathbf{u} \cdot \nabla \phi = \frac{1}{P e_{\phi}} \nabla^2 \mu_{\phi}$$

Chemical potential (Ginzburg-Landau theory)

$$\mu_{\phi} = \phi^3 - \phi - Ch^2 \nabla^2 \phi$$

Dimensionless parameters:

$Ch = \frac{\epsilon}{h}$	$Pe_{\phi} = rac{u_{ au}h}{\mathcal{M}eta}$
$Ch = \mathcal{O}(10^{-9})$	$Pe = \mathcal{O}(10^9)$
Cahn number	Peclet number

To reduce the computational effort, the interface must be fictitiously enlarged to the point that it becomes computationally tractable (3-5 grid poir

Jacqmin, Calculation of Two-Phase Navier–Stokes Flows Using Phase-Field Modeling, JCP (1999) Cahn and Hilliard , Free energy of a non-uniform system I, Interfacial free energy, JCP (1958) Roccon et al. "Phase-field modeling of complex interface dynamics in drop-laden turbulence, PRF (2023).

Multiphase turbulence Phase-field method (details)

Phase indicator ϕ











Numerical method:

- Wall-normal velocity formulation for the Navier-Stokes equations.
- Pseudo-spectral method (Fourier for the homogenous directions and Chebychev for the wall-normal direction)
- For Cahn-Hilliard equation, splitting technique (recasted in two 2nd order equations)

Parallelization strategy:

- First layer of parallalization that relies on MPI (2D domain decomposition), in -house library for pencil rotations. Used for CPU-based machines (Discoverer, LUMI-C, etc.) + FFTW.
- Second layer of parallelisation that relies on openACC directives and CUDA Fortran instructions for GPU-based machines (Leonardo) + cuFFT.

Multiphase turbulence Numerical method, parallelisation + GPU-acceleration and initial conditions

Initial conditions:

- Flow Field: (Shear Reynolds Re= 300)
- Phase Field and temperature: (adiabatic)



Fully developed turbulent channel flow

256 spherical hot drops in a cold channel

Simulation parameters:



Four different Prandtl numbers:

• Pr=1, 2, 4, 8 (obtained reducing therm. diff.)

Multi resolution strategy to resolve the Batchelor scale.

	Batchelor scale		
$Pr \rightarrow$	Pr	η_B	
	1	η_k	
η_k	2	$0.71\eta_k$	
$\left \frac{\eta_B}{\sqrt{Pr}} \right $	4	$0.50\eta_k$	
· · · · · · · · · · · · · · · · · · ·	8	$0.35\eta_k$	

Grid 1: 1024 x 512 x 513 Grid 2: 2048 x 1204 x 513















Roccon et al., "Phase-field modeling of complex interface dynamics in drop-laden turbulence, PRF (2023). Mangani et al., "Heat-transfer in drop-laden turbulence", JFM (2023)

Qualitative view Heat transfer process













Roccon et al., "Phase-field modeling of complex interface dynamics in drop-laden turbulence, PRF (2023). Mangani et al., "Heat-transfer in drop-laden turbulence", JFM (2023)

Qualitative view Time evolution (Pr=1)

Channel mid plane



Momentum diffusivity ν Pr = - =Thermal diffusivity a











Roccon et al., "Phase-field modeling of complex interface dynamics in drop-laden turbulence, PRF (2023). Mangani et al., "Heat-transfer in drop-laden turbulence", JFM (2023)

Qualitative view Time evolution (Pr=8)

Channel mid plane



















$$\theta_{eq}^{+} = \theta_{c,0}^{+}(1-\Phi) + \theta_{d,0}^{+}\Phi$$

Steady average temperature of the mixture

Volume fraction: $\Phi = 5.4\%$

Momentum diffusivity Pr = - =Thermal diffusivity a

Quantitative results Mean temperature

Drops can coalescence and break, and thus can have different sizes... What is the effect of drop size on temperature evolution?














Mangani et al., "Heat-transfer in drop-laden turbulence", JFM (2023)









Time evolution of average drop temperature for different drop sizes.



Momentum diffusivity ν Pr = -Thermal diffusivity a

down is faster







Bubbles/Drops break if stresses win over restoring surface tension

$$v_2$$

Kolmogorov-Hinze Critical radius

$$r_H \propto \left(\frac{\rho}{\sigma}\right) \varepsilon^{-2/5} \propto W e^{-3/5} \varepsilon^{-2/5}$$

$$V e^{-3/5} \varepsilon^{-2/5}$$

$$W e^{-3/5} \varepsilon^{-2/5}$$

$$W e^{-3/5} \varepsilon^{-2/5}$$

Small drops/bubbles

$$N(r) \propto Q\left(rac{\sigma}{
ho}
ight)^{-3/2} u^2 r^{-3/2}$$

Large drops/bubbles

$$N(r) \propto Q \varepsilon^{-1/3} r^{-10/3}$$

Roccon et al., "Phase-field modeling of complex interface dynamics in drop-laden turbulence, PRF (2023). Mangani et al., "Heat-transfer in drop-laden turbulence", JFM (2023)

Dispersed phase Drop size distribution



The steady-state size distribution well matches with the analytical scaling laws proposed in literature.







Thermal balance for an isolated drop:

$$m_d^* c_p^* \frac{\partial \theta_d^*}{\partial t^*} = \mathcal{H}^* A_d^* \left(\theta_c^* - \theta_d^* \right)$$

$$\mathcal{H}^*$$

$$\frac{\partial \theta_d^*}{\partial t^*} = \frac{6\nu^* \rho_c^*}{\rho_d^* d^* \delta_t^* P r} \left(\theta_c^* - \theta_d^*\right)$$

Temperature evolution for a single droplet:

$$\frac{\partial \theta_d^+}{\partial t^+} = \mathcal{C}Pr^{-2/3} \left(D_d^+ \right)^{-1} \left(\theta_f^+ - \theta_d^+ \right)$$
 Drop

We can now integrate this temperature evolution equation over different class of diameters (DSD) so as to obtain the evolution of the mean temperature of the drops and of the carrier flow.

Simple model for mean temperature evolution (I)

Boundary layer theory (heat transfer coefficient):











Roccon et al., "Phase-field modeling of complex interface dynamics in drop-laden turbulence, PRF (2023). Mangani et al., "Heat-transfer in drop-laden turbulence", JFM (2023)

Excellent agreement between the numerical results and the phenomenological model...!!

We can also rescale everything using the Pr^2/3 exponent and collapse all the curves:











Conclusions:

- The heat transfer from the drops to the carrier fluid shows an expected dependency on *Prandtl*: the higher is the Pr, the slower is the diffusion and thus the heat transfer between the phases
- We developed an analytical model which can well predict the average temperature of the two phases
- We found a scaling for the time (diffusive time)
- We found a correlation between the diameter and the average temperature

Future developments:

- Extend the simulations to mass/species transfer.
- Thermocapillary Marangoni effects
- Phase Change/Boiling (MIT Collaboration)



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Conclusions & Future developments



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